Plume-SPH 1.0: A three-dimensional, dusty-gas volcanic plume model based on smoothed particle hydrodynamics

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Abstract.

Plume-SPH provides the ~~the~~ the first particle based simulation of volcanic plumes. SPH (smoothed particle hydrodynamics) has several advantages over currently used mesh based methods in modeling of multiphase free boundary flows like volcanic plumes. This tool will provide more accurate eruption source terms to users of VATDs (Volcanic ash transport and dispersion models) greatly improving volcanic ash forecasts. The accuracy of these terms is crucial for forecasts from VATDs and the 3D SPH model presented here will provide better numerical accuracy. As an initial effort to exploit the feasibility and advantages of SPH in volcanic plume modeling, we adopt a relatively simple physics model (3D dusty-gas dynamic model assuming well mixed eruption ~~materiel~~ and dynamic and thermodynamic equilibrium between air and erupted material and minimal effect of winds) targeted at capturing the salient features of a volcanic plume. The documented open source code is easily obtained and extended to incorporate other models of physics of interest to the large community of researchers investigating multiphase free boundary flows of volcanic or other origins.

The Plume-SPH code also incorporates several newly developed techniques in SPH needed to address numerical challenges in simulating multiphase compressible turbulent flow. The code should thus be also of general interest to the much larger community of researchers using and developing SPH based tools. In particular, the $SPH - \varepsilon$ turbulence model is to capture mixing at unresolved scales. heat exchange due to turbulence is calculated by a Reynolds analogy and a corrected SPH is used to handle tensile instability and deficiency of particle distribution near the boundaries. we also developed methodology to impose velocity inlet and pressure outlet boundary conditions, both of which are scarce in traditional implementations of SPH.

The core solver of our model is parallelized with MPI (message passing interface) obtaining good weak and strong scalability using novel techniques for data management using a SFCs (space-filling curves) and object creation time based indexing and hash table based storage scheme. These techniques are of interest to researchers engaged in developing particle in cell type methods. The model is verified by comparing velocity and concentration distribution along the central axis and on the transverse cross with experimental results of JPUE (jet or plume that is ejected from a nozzle into a uniform environment) and the top height of the Pinatubo eruption of 15 June 1991. Our results are consistent with both observations and existing 3D plume models. Profiles of several integrated variables are compared with those calculated in existing 3D plume models, and further

verify our model. Analysis of the plume evolution process illustrates that this model is able to reproduce the physics of plume development.

1   Introduction

1.1   Volcanic ash hazards

5   Primary hazards associated with explosive volcanic eruptions include pyroclastic density currents (flows and surges), the widespread deposition of airfall tephra, and the threats to aviation posed by volcanic ash in the atmosphere. Simulation of all possible hazards with one model is difficult due to the fact that different length scales dominate different hazards. Our focus here is the hazard that volcanic ash poses to aircraft.

During volcanic eruptions, VATDs (volcanic ash transport and dispersion models) are used to forecast the location and
10   movement of ash clouds at timescales that range from hours to days. VATDs use eruption source parameters, such as plume height, mass eruption rate, duration, and the mass fraction distribution of erupted debris finer than about 4Φ (or 63μm), which can remain in the cloud for many hours or days. Observational data for such parameters are usually unavailable in the first minutes or hours after an eruption is detected. Moreover, these input parameters are subject to change during an eruption, requiring rapid re-assignment of new parameters. Usually, plume models are used to provide these source terms for VATDs
15   and the forecast accuracy is critically dependent on these models. This paper reports on a new 3D (three dimensional) volcanic plume model designed to exploit the advantages of mesh-free methods for 3D modeling of such plumes that involve multiphase free boundary flows.

1.2   Existing plume models

Several 1D (one dimensional) volcanic plume models have been developed in the past few decades, ranging from the most
20   basic 1D model (Woods, 1988) which only accounts for mass conservation to more recently developed 1D models (Bursik, 2001; Mastin, 2007; Degruyter and Bonadonna, 2012; Woodhouse et al., 2013; Devenish, 2013; de'Michieli Vitturi et al., 2015; Folch et al., 2016; Pouget et al., 2016) which tend to account for more comprehensive physics effects. For example, FPLUME-1.0 (Folch et al., 2016) accounts for wind effect, entrainment of moisture, water phase change, particle fallout and re-entrainment and even wet aggregation of ash. However, in these 1D models, the entrainment of air is evaluated based on
25   two coefficients: entrainment coefficient for the vertical plume and the entrainment coefficient that describes the effect of wind. Different 1D models adopt different entrainment coefficients based on specific formulation or calibration against well-documented case studies. The feedback from plume to atmosphere is usually ignored in 1D models. Even though determination of essential parameters such as the entrainment is not based on first principles, such simple models nevertheless allow us to investigate the importance of physical mechanisms in a volcanic plume. In addition, these simplified models require little
30   computational resource and can run on standard personal computers or on web sites in very short time. As a result, 1D software for volcanic plume development (such as Bursik, 2010; Mastin, 2011; Vitturi, 2015), combined with VATDs (such as Bursik

et al., 2013; Draxler and Rolph, 2015) are widely used in research and practice. While these 1D models can generate well-matched results with 3D (three dimensional) models for weak plumes, much greater variability is observed for strong plume scenarios, especially for local variables (Costa et al., 2016). In addition, there is need for greater skills in hazards forecasts especially where the plume model is used to generate source conditions for complex 2D (two dimensional) and 3D VATD

5   models.

The development of 2D and 3D, time-dependent, and multiphase numerical models for volcanic plumes has provided new explanations for many features of explosive volcanism. One of the earliest of these is the 3D model PDAC (Pyroclastic Dispersion Analysis Code) (Neri et al., 2003) which is a non-equilibrium, multiphase, 3D compressible flow model. Conservation equations for each phase are solved separately with the finite volume method. A parallel computing version of PDAC was

10   also developed (Ongaro et al., 2007). Advanced numerical techniques, such as a second order scheme and semi-explicit time stepping, was also adopted afterwards to improve the accuracy of PDAC (Carcano et al., 2013).

Another 3D model, SK-3D (Suzuki et al., 2005) is a 3D time-dependent fluid dynamics model that attempts to reproduce the entrainment process of eruption clouds with relatively simple physics but with high order numerical accuracy and high spatial resolution. A series of simulations based on SK-3D was reported, including establishment of the relationship between the

15   observable quantities of the eruption clouds and the eruption conditions at the vent (Suzuki and Koyaguchi, 2009), investigation of the effect of the intensity of turbulence in the umbrella cloud on dispersion and sedimentation of tephra (Koyaguchi et al., 2009), determination of the entrainment coefficients of eruption columns as a function of height (Suzuki and Koyaguchi, 2010) and investigation of the effect of wind field on entrainment coefficient (Suzuki and Koyaguchi, 2013).

While SK-3D focuses on accurately capturing the entrainment caused by turbulent mixture with higher resolution and

20   numerical method of higher order, PDAC takes the disequilibrium between different phases into account and hence is a true multiphase model. Another 3D model, ATHAM (Active Tracer High-Resolution Atmospheric Model) (Oberhuber et al., 1998) focuses more on microphysics within the plume. As pyroclastic flow is not the initial concern of ATHAM, dynamic and thermodynamical equilibrium is assumed in ATHAM. The dynamic core of ATHAM solves the compressible Euler equations for momentum, pressure and temperature of the gas particle mixture (Oberhuber et al., 1998). The subgrid-scale turbulence

25   closure scheme differentiates between the horizontal and vertical directions (Herzog et al., 2003) captures turbulent mixing. The cloud microphysics predicts the mass of hydrometeors in liquid and ice phase (Herzog et al., 1998). Additional modules, including gas phase chemistry (Trentmann et al., 2002) and gas scavenging by hydrometeors (Textor et al., 2003) were added lately. A further extension was made to include particle aggregation (Textor et al., 2006b, a). However, the resolution of ATHAM is still coarse compared with SK-3D and PDAC.

30   Besides adding to their special strengths (ATHAM has been adding more and more microphysics, PDAC was extended to consider more phases), these models are also adding core strengths. PDAC development has begun to include the effect of microphysics into the model while ATHAM development has extended its ability to modeling pyroclastic flow. Both are using finer and finer resolution.

Recently, a first order, nonequilibrium compressible 3D model, ASHEE (Cerminara et al., 2016a), was introduced based on

35   three dimensional N-phases Eulerian transportation equations, which are a full set of mass, momentum and energy transport

equations for a mixture of gas and dispersed particles. ASHEE is valid for low concentration and low Stokes number region and much faster than N-phases Eulerian model. The model is based on the open source numerical solver OpenFOAM (Weller et al., 1998), adapting its unstructured finite volume solver.

To summarize, each 3D model has its own focus based on the problem of interest and modeling/numerical choices made.
5 Accuracy of simulation (depending on comprehensiveness of the model, resolution of discretization, numerical error, and order of accuracy) and simulation time (depending on number of governing equations, resolution, numerical methods and parallel techniques) are always a pair of conflicting considerations in 3D plume simulations.

1.3 Features of SPH

10 To the best of our knowledge, all of the existing 3D plume models use mesh based Eulerian methods, and there are no 3D plume models based on mesh free Lagrangian methods. Lagrangian methods have several features that are suitable for volcanic plume simulation that we outline below. Among such Lagrangian methods, smoothed particle hydrodynamics (Gingold and Monaghan, 1977; Lucy, 1977) based simulations have shown good agreement with experiments for many applications in fluid dynamics. And it currently is, by far, the most widely used mesh-free scheme. Our implementations of SPH in volcanology
15 follows on earlier efforts (Bursik et al., 2003; Hérault et al., 2010; Haddad et al., 2016). Specifically, we choose SPH as the numerical method for volcanic plume simulation to enable:

- better investigation of mixing phenomena;

- accurate modeling of the development of ZFE (Zone of Flow Establishment), ZEF (Zone of Established Flow) investigation and relation to column collapse and the questions relating to the development of entrainment;

20 - easy inclusion of particles of different sizes (phases) and investigation of detailed mechanics of sedimentation and drag force interaction in lower plume.

These are enabled by the following features of SPH:

- For mesh based method, either interface tracking (Lagrangian) (Harlow et al., 1965; Wrobel and Brebbia, 1991; Cheng and Armfield, 1995) or interface capturing (Eulerian) (Hirt and Nichols, 1981; Youngs, 1982; Gerlach et al., 2006; Gopala
25 and van Wachem, 2008) methods are used to reconstruct the flow interface of free boundary flow. High computational cost, a tendency to form numerical instabilities and the inability to track complex topological changes are the significant drawbacks of tracking techniques (Hirt and Nichols, 1981; Unverdi and Tryggvason, 1992; Anderson et al., 1998). For interface capturing (Eulerian) method, the surrendering of surface detail before the phase transport calculation means that interface reconstruction is required between time steps to recover the interface information, which needs additional
30 numerical effort (Hirt and Nichols, 1981; Youngs, 1982). Since SPH is able to adaptively adjust the discretization and automatically construct the interface, SPH does not require additional numerical effort for interface construction and therefore is more suitable for volcanic plume simulation.

- Advection term in the Navier-Stokes equations does not appear explicitly in discretized formula of SPH (as illustrated in Eq. (12) to Eq. (15)).

- It is easy to include various physics effects (like self gravity, radiative cooling and chemical reaction) into the model. It does not require a major overhaul and re-tooling every time new physics is introduced (Monaghan and Kocharyan, 1995). This implies that accounting for more physics is easier for SPH model.

- With more than one material, each described by its own set of particles, interface problems between phases are often trivial for SPH but difficult for mesh based schemes. So multiphase flow can be easily handled by SPH. Adding of new phases to the model also does not require a major overhaul and re-tooling. As will be shown in later paragraphs, adding of new phases only leads to adding of several lines into the source code for new phases and additional interaction terms between existing phases and newly added phases.

As discussed in the previous paragraph, existing 3D plume models focus on one or several specific aspects of plume and have been extended to be more comprehensive by accounting for more physics or more phases. Easy extensibility and capability of handling multiples phase flow without additional numerical effort greatly facilitate future extension of SPH models. As volcanic plumes are in nature multiphase and without pre-defined boundary in the atmosphere, SPH is a suitable numerical method for plume modeling. The core physics, such as entrainment of air and thermal expansion, are essential for all plume modeling while some other physics, such as water condensation and aggregation etc., are important in specific scenarios. As an initial effort on exploiting advantages of SPH in volcanic plume modeling, we focus on capturing basic features in plume development using a robust numerically and computationally efficient framework with support for scalable parallel computing.

Open source availability and the relatively easy extensibility of SPH will facilitate development of a more comprehensive community driven model.

1.4 Our contributions

Even though SPH has been known for several decades, implementations of SPH for compressible multiphase turbulent flows are few. Several issues endemic to classical SPH, like tensile instabilities, compressible turbulence modeling and turbulent heat exchange, are fixed in our implementation. The most popular applications of SPH (and their original motivating application) has been in the simulation of free surface flow, such as breaking-waves and floods. Less attention was paid to velocity inlet and pressure outlet boundary conditions which are required in plume modeling.

- We develop methodology to impose pressure boundary conditions by adding extra layers of static ghost particles. Additional constraints on the time step is used to avoid the growth of numerical fluctuations near the pressure boundary. We impose a velocity inlet boundary condition by placing several layers of ghost particles moving with eruption velocity.

- Turbulence model is crucial for reproducing the entrainment of air. There are several turbulence models proposed for SPH method (Issa, 2005; Violeau and Issa, 2007). We adopt a LANS (Lagrangian Averaged Navier-Stokes) turbulence

model (Monaghan, 2011), which was originally proposed for incompressible flow, and is extended here for compressible flow accounting for turbulent heat exchange.

– Corrected formulation of SPH (Chen et al., 1999) is adapted to bypass the well-known tensile instability issues of classical SPH.

5 – Simulation of volcanic plumes with acceptable accuracy requires fine resolution (very high particle counts) that cannot be accomplished without parallel computing. The core solver of our model is parallelized by MPI (message passing interface standard) parallelism. In addition, a dynamic load balancing strategy is also developed.

– Imposition of some types of boundary conditions (such as eruption boundary condition) requires dynamically adding and removing of particles during simulation. To address this issue, we adopt an efficient data management scheme based 10 on time dependent SFC (space filling curve) induced indexing and hash table. The computational cost is further reduced by adjusting simulation domain adaptively.

The physical model of the plume is first presented in section 2 and leads to a complete mathematical description of the volcanic plume (governing equations and boundary conditions). In section 3, we briefly introduce the numerical tool – the SPH method. Both the fundamental discretization formulation and techniques that are used to handle specific issues involved 15 in plume modeling are discussed. Verification and validation with numerical tests are presented in section 4. In section 5, a discussion on future work is given following a brief summary.

2 Physical model

2.1 Description of the model

During an explosive eruption, a volcanic jet erupts out from a vent with a speed of several tens to more than 150 meters per 20 second, driven by expanding gas. The jet is initially denser than the surrounding atmosphere and begins to decelerate through negative buoyancy and turbulent interaction with surrounding air. Cauliflower-like vortices are generated along jet margins, within which process, air is entrained and heated up, reducing the bulk density of the entire jet, in many cases, to less than that of the surrounding atmosphere. Once it becomes buoyant, such a jet develops into a plinian or subplinian plume, rising up to several kilometers to tens of kilometers until its heat is exhausted. Jets that lose their momentum before becoming buoyant 25 collapse back onto the ground and transform into pyroclastic flows, surges and ignimbrites. During the process of plume rising up, relatively larger particles might separate from main stream of the plume, falling down onto the ground and probably be re-entrained into the plume at a lower height (Ernst et al., 1996). Within this process, erupted vapor condenses to liquid (droplet) and even further to ice. Latent heat released from phase change of erupted vapor further heats up entrained air and further dilutes the bulk density. The entrained vapor might also experience a similar process and impact plume development. Particle 30 aggregation processes (Carey and Sigurdsson, 1982; Taddeucci et al., 2011), either due to presence of liquid water, resulting from particle collision or driven by electrostatic forces might occur inside plume and thereby affect the sedimentation.

All in all, the process of plume development is essentially a multiphase turbulent mixing process coupled with heat transfer and other microphysical and chemical reactions.

As an initial effort on exploiting the feasibility and advantage of SPH in plume modeling, our model is designed to describe an injection of well mixed solid and volcanic gas from a circular vent above a flat surface into a stratified stationary atmosphere following SK-3D (Suzuki et al., 2005). In this model, molecular viscosity and heat conduction is neglected since turbulent exchange coefficients are dominant. Erupted material consisting of solid with different size and mixture of gases is assumed to be well mixed and behave like a single phase fluid (phase 2) which is valid for eruptions with fine particles and ash. Air (also a mixture of different gases) is assumed to be another phase (phase 1). Thermodynamic equilibrium is assumed so that no separate energy equation is needed for each phase. As a result, there is only one energy equation for both phases (heat exchange term between different phases does not show up under this assumption). Dynamic equilibrium is assumed so that no separate momentum equation is needed for each phase. As a result, there is only one vector momentum equation for both phases (drag force term does not show up with this assumption).

Because of the above assumptions, all other microphysical processes (such as the phase changes of H_2O aggregation, disaggregation, absorption of gas on the surface of solids, solution of gas into a liquid) and chemical processes are not considered in this model. These ignored microphysics factors would play critical roles under particular eruption conditions. Capturing of these processes needs a more comprehensive model. One critical element in plume development, the effect of wind, is also not yet considered in this model. Introducing wind effects in our model requires dynamic pressure boundary conditions, which requires more numerical effort and algorithm design. To summarize, our model is not valid for eruptions where wind effect plays a significant role in its development, usually refered as a weak plume. Our model also lacks the ability in modeling plumes with large particles or eruptions in which microphysics plays non-ignorable roles, such as a eruption of *El Chichón* volcano on April 4th 1982 (Sigurdsson et al., 1984; Folch et al., 2016). We are focussed here on developing the SPH based methodoloy in the context of the more basic (and more critical) aspects of volcanic plume and therefore devote our effort to this relative simpler model. It is worthwhile to mention here that because SPH is adopted as our numerical method, adding of these physics into our model would require much less work in terms of programming compared to mesh based methods. Since our plan is an open source distribution of the tool we believe some of these enhancements will rapidly ensue with community participation.

2.2 Governing equations

Based on above assumptions, the governing equations of our model are given as (which is the same as the governing equations of SK-3D (Suzuki et al., 2005)):

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{v}) = 0 \tag{1}$$

$$\frac{\partial \rho \xi}{\partial t} + \nabla \cdot (\rho \xi \mathbf{v}) = 0 \tag{2}$$

$$\frac{\partial \rho \mathbf{v}}{\partial t} + \nabla \cdot (\rho \mathbf{v} \mathbf{v} + p \mathbf{I}) = \rho \mathbf{g} \tag{3}$$

$$\frac{\partial \rho E}{\partial t} + \nabla \cdot [(\rho E + p) \mathbf{v}] = \rho \mathbf{g} \cdot \mathbf{v} \tag{4}$$

Where ρ is the density, $\mathbf{v}$ is the velocity, ξ is the mass fraction of ejected material, $\mathbf{g}$ is the gravitational acceleration, $\mathbf{I}$ is a unit tensor. $E = e + K$ is the total energy which is a summation of kinetic energy K and internal energy e. An additional equation is required to close the system. In this model, the equation for closing the system is the following EOS (equation of state).

$$p = (\gamma_m - 1)\rho e \tag{5}$$

5 Where

$$\gamma_m = R_m / C_{vm} + 1 \tag{6}$$

$$R_m = \xi_g R_g + \xi_a R_a \tag{7}$$

10 $$C_{vm} = \xi_s C_{vs} + \xi_g C_{vg} + \xi_a C_{va} \tag{8}$$

$$\xi_a = 1 - \xi \tag{9}$$

$$\xi_g = \xi \cdot \xi_{g0} \tag{10}$$

$$\xi_s = \xi - \xi_g \tag{11}$$

Where, C_v is the specific heat with constant volume, R is the gas constant. ξ with subscript is the mass fraction of corresponding constituent. The subscript m represents mixture of ejected material and air, s represents solid portion in the ejected material, g represents gas portion in the ejected material and a represents air. ξ_{g0} is the mass fraction of vapor in the erupted material.

20   In mesh based methods, governing equations in Eulerian form, Eq. (1) to Eq. (4), are directly discretized. For SPH, governing equations in Lagrange form are needed. By deducting kinetic energy from energy equation, subtracting mass conservation from momentum equation, combining transient term and advection term into material derivative term, the governing equations are put into the final form, in which advection term does not appear explicitly.

$$\frac{D\rho}{Dt} + \rho \nabla \cdot \mathbf{v} = 0 \tag{12}$$

25 $$\frac{D\rho\xi}{Dt} + \rho\xi \nabla \cdot \mathbf{v} = 0 \tag{13}$$

$$\frac{D\mathbf{v}}{Dt} + \frac{\nabla P}{\rho} = \mathbf{g} \tag{14}$$

$$\frac{De}{Dt} + \frac{P\nabla \cdot \mathbf{v}}{\rho} = 0 \tag{15}$$

2.3 Boundary conditions

In the current model the initial domain is a box. The boundaries are categorized as the velocity inlet (a circular area at the center of the bottom of the box), wall boundary (box bottom), pressure outlet (other faces of the box).

2.3.1 Velocity inlet

5   At the vent, temperature of erupted material T, eruption velocity $\mathbf{v}$, the mass fraction of vapor in erupted material ξ_{g0} and mass discharge rate $\dot{M}$ are given. The pressure of erupted material p is assumed to be the same as ambient pressure for pressure-balanced eruption. The radius of vent is determined from ρ, $\dot{M}$ and $\mathbf{v}$. Equation (16) to (19) gives velocity outlet boundary condition wrote in terms of primitive variables.

$$\rho = const = p/\left(R_m T\right) \tag{16}$$

$$\xi = const = 1 \tag{17}$$

$$\mathbf{v} = const = \{u, v, w\}^T \tag{18}$$

$$\frac{\partial e}{\partial n} = \dot{M} e / \left(\pi r^2\right) \tag{19}$$

Where r is the radius of the vent, n is the direction normal to the boundary.

2.3.2 Non-slip wall boundary

15   Velocity is zero for non-slip wall boundary. If we assume the boundary to be adiabatic, heat flux should be zero on the boundary. The flux of mass should also be zero. As a result, internal energy flux, which consists of heat flux and energy flux carried by mass flux, vanishes on the wall boundary. Equation (20) to (23) gives no-slip wall boundary condition written in terms of primitive variables.

$$\frac{\partial \rho}{\partial n} = const = 0 \tag{20}$$

$$\frac{\partial \xi}{\partial n} = const = 0 \tag{21}$$

$$\mathbf{v} = const = \{0, 0, 0\}^T \tag{22}$$

$$\frac{\partial e}{\partial n} = 0 \tag{23}$$

2.3.3 Open outlet pressure boundary condition

The pressure of the surrounding atmosphere is given. Except for the pressure, boundary values for density, velocity, and energy

25   on the outlet should depend on the solution. As we ignore the viscosity, the shear stress is ignored and normal stress (whose magnitude equals to pressure) balances the ambient pressure.

$$p = p_a \left(z\right) \tag{24}$$

3 SPH method

SPH is a mesh-free Lagragian method. In SPH, the domain is discretized by a set of particles or discretization points and the position of each particle is updated at every time step based on the motion computed. Approximation of all field variables (velocity, density and pressure, ect.) is obtained by interpolation based on discretization points. The physical laws (such as
5   conservation laws of mass, momentum and energy) written in the form of PDEs (partial differential equations) or ODEs (ordinary differential equations) need to be transformed into the Lagrangian particle formalism of SPH. Using a kernel function that provides the weighted estimation of the field variables at any point, the integral equations are estimated as sums over particles in a compact subdomain defined by the support of the kernel function associated with the discretization points. Thus, field variables associated to the particle are updated based on its neighbors. Each kernel function has a compact support
10   determined by smoothing length of each particle. There are several review papers by Monaghan (1992, 2005); Rosswog (2009); Price (2012); Monaghan (2012), giving a pretty comprehensive view over SPH. We only refer here to the representation of the constitutive equations in SPH and put more focus on specific numerical techniques for plume modeling.

3.1 Fundamental principles

There are several procedures for discretizing governing equations (PDEs or ODEs) with SPH. We present here one of them
15   following Monaghan (1992, 2005, 2012). The starting point of approximating a function with SPH is the translation property of the Dirac function.

$$A(\mathbf{x}) = \int_{-\infty}^{\infty} A(\mathbf{x}\prime)\,\delta(\mathbf{x}\prime - \mathbf{x})\,d\mathbf{x}\prime \tag{25}$$

The Dirac function in Eq. (25) can be approximated by a weighting function $w(\mathbf{x} - \mathbf{x}\prime, h)$ (or $w(\mathbf{x}\prime - \mathbf{x}, h)$)) which tends to a Dirac function when the smoothing length $h \to 0$:

20   $$\lim_{h \to 0} w(\mathbf{x}\prime - \mathbf{x}, h) = \delta(\mathbf{x}\prime - \mathbf{x}) \tag{26}$$

An arbitrary function $A(\mathbf{x})$ can then be approximated by:

$$A(\mathbf{x}) \approx\,< A(\mathbf{x}) >= \int A(\mathbf{x}\prime)\,w(\mathbf{x} - \mathbf{x}\prime, h)\,d\mathbf{x}\prime + O(h^2) \tag{27}$$

Where h is the smoothing length, determining the interaction distance. As the weighting function is symmetric (Eq. (35)) and satisfies the normalization condition (Eq. (34)), odd error terms in Eq. (27) vanishe leading to a second order approximation.
25   However, in practice, second order of accuracy can not be achieved because there is no guarantee on the symmetry of particle distribution in real simulation (Price, 2012). Recall that $d\mathbf{x}\prime = \dfrac{dm\prime}{\rho\prime}$, the integration equation, Eq. (27), can be approximated by summation and lead to an approximation of the function A:

$$< A(\mathbf{x}) >\approx \sum_b m_b \frac{A_b}{\rho_b} w(\mathbf{x} - \mathbf{x}_b, h) \tag{28}$$

where the summation is over all the particles within the region of compact support of the weighting function. Gradient terms may be straightforwardly calculated by taking the derivative of Eq. (28), giving

$$< \nabla A(\mathbf{x}) > = \frac{\partial}{\partial \mathbf{x}} \int_{\Omega} A(\mathbf{x}\prime) \, w(\mathbf{x} - \mathbf{x}\prime, h) \, d\mathbf{x}\prime + O(h^2)$$

$$\approx \sum_b m_b \frac{A_b}{\rho_b} \nabla w(\mathbf{x} - \mathbf{x}_b, h) \tag{29}$$

For vector quantities the expressions are similar, simply replacing A with $\mathbf{A}$ in Eq. (28) and Eq. (29), giving

$$< \mathbf{A}(\mathbf{x}) > \approx \sum_b m_b \frac{\mathbf{A}_b}{\rho_b} w(\mathbf{x} - \mathbf{x}_b, h) \tag{30}$$

$$< \nabla \cdot \mathbf{A}(\mathbf{x}) > \approx \sum_b m_b \frac{\mathbf{A}_b}{\rho_b} \cdot \nabla w(\mathbf{x} - \mathbf{x}_b, h) \tag{31}$$

$$< \nabla \times \mathbf{A}(\mathbf{x}) > \approx \sum_b m_b \frac{\mathbf{A}_b}{\rho_b} \times \nabla w(\mathbf{x} - \mathbf{x}_b, h) \tag{32}$$

$$< \nabla^j \mathbf{A}^i(\mathbf{x}) > \approx \sum_b m_b \frac{\mathbf{A}_b^i}{\rho_b} \nabla^j w(\mathbf{x} - \mathbf{x}_b, h) \tag{33}$$

3.2 Weighting function

As described in the previous section, the weighting function (or kernel function) is used to replace the Dirac function and should satisfy Eq. (26). So it can be viewed as an approximate form of the Dirac function and satisfies the normalization condition:

$$\int w(\mathbf{x} - \mathbf{x}\prime, h) \, d\mathbf{x}\prime = 1 \tag{34}$$

Besides normalization, the weighting function of particle a has to be symmetric with respect to a to ensure that neighbor particles located at the same distance away from a contribute equally to SPH summation equation, see Eq. (35). The weighting function also needs to satisfy conditions such as positivity and compact support. In addition, the kernel function must be monotonically decreasing with the distance between particles.

$$w(\mathbf{x} - \mathbf{x}\prime, h) = w(\mathbf{x}\prime - \mathbf{x}, h) \tag{35}$$

There is a wide variety of possible weighting functions, such as spline functions (with different orders) and Gaussian functions. Generally, the accuracy increases with the order of the polynomials of the kernel function, but the computational cost also increases as number of interactions increase. We are adopting a truncated Gaussian function as the weighting function in our simulation.

$$w(\mathbf{x} - \mathbf{x}_b) = \begin{cases} \dfrac{1}{(h\sqrt{\pi})^d} exp\left[-\left(\dfrac{\mathbf{x} - \mathbf{x}\prime}{h} \right)^2 \right] & |\mathbf{x} - \mathbf{x}\prime| \leq 3h \\ 0 & \text{Otherwise} \end{cases} \tag{36}$$

Where d is number of dimensions. The derivative of the weighting function:

$$\nabla w\left(\mathbf{x} - \mathbf{x}_b\right) = \begin{cases} -2\left(\dfrac{\mathbf{x} - \mathbf{x}\prime}{h^2}\right) \dfrac{1}{\left(h\sqrt{\pi}\right)^d} exp\left[-\left(\dfrac{\mathbf{x} - \mathbf{x}\prime}{h}\right)^2\right] & |\mathbf{x} - \mathbf{x}\prime| \le 3h \\ 0 & \text{Otherwise} \end{cases} \tag{37}$$

3.3 Discretization of governing equations and extensibility

The basic interpolation given in Eq. (28) to Eq. (33) provides a general way to obtain SPH expressions of governing equations. The problem is that using these expressions "as is" in general leads to quite poor gradient estimates. Various tricks can be used to conserve linear and angular momentum and thermal energy (Monaghan, 1992). Special treatments are also needed for second order derivative terms (Monaghan, 2005). We only refer here to one of these possible discretizations of compressible Euler equations with SPH:

$$< \rho_a > = \sum_b m_b w_{ab}\left(h\right) \tag{38}$$

$$\left\langle \frac{d\mathbf{v}_a}{dt} \right\rangle = -\sum_b m_b \left(\frac{p_b}{\rho_b^2} + \frac{p_a}{\rho_a^2} + \Pi_{ab}\right) \nabla_a w_{ab}\left(h\right) + \mathbf{g} \tag{39}$$

$$\left\langle \frac{de_a}{dt} \right\rangle = 0.5 \sum_b m_b \mathbf{v}_{ab} \left(\frac{p_b}{\rho_b^2} + \frac{p_a}{\rho_a^2} + \Pi_{ab}\right) \cdot \nabla_a w_{ab}\left(h\right) \tag{40}$$

where, a is the SPH particle index, $\mathbf{v}_{ab} = \mathbf{v}_a - \mathbf{v}_b$. Π is an artificial viscosity term, which will be discussed in section 3.4. $w_{ab}\left(h\right)$ is a concise form of $w\left(\mathbf{x}_a - \mathbf{x}_b, h\right)$ and from here on, we will use this concise form. As a Lagrangian method, particle position is also updated at every time step.

$$\left\langle \frac{d\mathbf{x}_a}{dt} \right\rangle = \mathbf{v}_a \tag{41}$$

We highlight an important feature of the SPH methodology. Adding new physics and new phases into the model is trivial in terms of discretization. For example, adding of new source (or sink) into Eq. (38), adding a drag force into Eq. (39) and adding a heat exchange term into Eq. (40) leads to the new discretization form:

$$< \rho_a > = \sum m_b w_{ab}\left(h\right) + \dot{\rho}\left(\mathbf{x}, t\right) \tag{42}$$

$$\left\langle \frac{d\mathbf{v}_a}{dt} \right\rangle = -\sum_b m_b \left(\frac{p_b}{\rho_b^2} + \frac{p_a}{\rho_a^2} + \Pi_{ab}\right) \nabla_a w_{ab}\left(h\right) + \mathbf{g} + D \sum_b m_b \frac{\mathbf{v}_b - \mathbf{v}_a}{\rho_b} \tag{43}$$

$$\left\langle \frac{de_a}{dt} \right\rangle = 0.5 \sum_b m_b \mathbf{v}_{ab} \left(\frac{p_b}{\rho_b^2} + \frac{p_a}{\rho_a^2} + \Pi_{ab}\right) \cdot \nabla_a w_{ab}\left(h\right) + \sum_b \frac{m_b}{\rho_b} \left(\kappa_a + \kappa_b\right) \frac{\left(T_a - T_b\right)}{\mathbf{r}_a - \mathbf{r}_b} w_{ab}\left(h\right) \tag{44}$$

where the source term $\dot{\rho}$ can be a "sink" of erupted vapor due to its phase change. D is a drag force coefficient. κ is the heat conduction coefficient. T is the temperature. Other physics can be added easily in a similar way. Adding of these new terms leads to modification of several lines in the source code. The drag force term should show up only when dynamics disequilibrium between different phases is considered that case, each phase needs one set of governing equations of Navier-Stokes type. Adding of new phase into SPH code only needs adding few new lines for the new phase besides interaction terms introduced by the new phase.

3.4 Artificial viscosity

In classical SPH, shock waves are handled by introducing artificial viscosity to smear out discontinuities. Π, in discretized momentum equation, Eq. (39), and energy equation, Eq. (40), represents artificial viscosity term which is essentially a second order derivative term. As in the case of first order derivatives, second order derivatives can be estimated by differentiating SPH interpolation twice. However, such a formulation has two disadvantages: First, it is very sensitive to particle disorder. Second, the second derivative of the kernel can change sign and lead to unphysical representations (For example, viscous dissipation causes decrease of the entropy).

One of the most commonly used models of artificial viscosity is:

$$\Pi_{ab} = -\frac{\nu}{\bar{\rho}_{ab}} \frac{\mathbf{v}_{ab} \cdot \mathbf{x}_{ab}}{\mathbf{x}_{ab}^2 + (\eta h)^2} \tag{45}$$

The coefficient ν is defined as:

$$\nu = \alpha \bar{h}_{ab} \bar{c}_{ab} \tag{46}$$

Where

$$\bar{c}_{ab} = \frac{c_a + c_b}{2} \tag{47}$$

$$\bar{\rho}_{ab} = \frac{\rho_a + \rho_b}{2} \tag{48}$$

$$\mathbf{v}_{ab} = \mathbf{v}_a - \mathbf{v}_b \tag{49}$$

$$\mathbf{x}_{ab} = \mathbf{x}_a - \mathbf{x}_b \tag{50}$$

The artificial viscosity term Π_{ab} is a Galilean invariant and vanishes for rigid rotation. It produces a repulsive force between two particles when they are approaching each other and an attractive force when they are receding from each other.

The SPH viscosity can be related to a continuum viscosity by converting the summation to integrals (Monaghan, 2005). It has been shown that the shear viscosity coefficient $\eta = \frac{\rho \alpha h c}{8}$ and the bulk viscosity coefficient $\zeta = \frac{5\eta}{3}$ for two dimensional and $\eta = \frac{\rho \alpha h c}{10}$, $\zeta = \frac{5\eta}{3}$ for three dimensional. An extra term was added to ν considering aspects of the dissipative term in shock solutions based on Riemann solvers and lead to a new formulation of artificial viscosity. We adopt this new formulation in our simulation:

$$\Pi_{ab}^{\beta} = \begin{cases} \dfrac{-\alpha \mu_{ab} \bar{c}_{ab} + \beta \mu_{ab}^2}{\bar{\rho}_{ab}} & \mathbf{v}_{ab} \cdot \mathbf{x}_{ab} < 0 \\ 0 & \mathbf{v}_{ab} \cdot \mathbf{x}_{ab} > 0 \end{cases} \tag{51}$$

Where

$$\mu_{ab} = \frac{h \mathbf{v}_{ab} \cdot \mathbf{x}_{ab}}{\mathbf{x}_{ab}^2 + (\eta h)^2} \tag{52}$$

α and β are two parameters that can be adjusted for different cases. $\alpha = 1$ and $\beta = 2$ are recommended by Monaghan for best results. In our simulation, these two parameters are calibrated to $\alpha = 0.3$ and $\beta = 0.6$. η is usually taken as 0.1 to prevent singularities.

3.5 Time step

The physical quantities (velocity, density and pressure) and particle position change every time step. The Courant condition, which is in spirit similar to the Courant condition for the mesh-based methods, is used to determine the time step Δt.

$$\Delta t = \text{CFL} \min_a \left\{ \frac{\left[\frac{m_a}{\rho_a} \right]^{\frac{1}{d}}}{c_a} \right\} \tag{53}$$

5   Where c_a is sound speed at particle a, d is number of dimensions. First order Euler integration, with CFL $= 0.2$, is used to advance in time.

3.6 Tensile instability and corrected derivatives

The classical SPH method was known to suffer from tensile instability and boundary deficiency. To address these difficulties, Chen (Chen et al., 1999) proposed a corrected SPH formulation. For 1D case, employing a Taylor expansion for $A(x)$ about

10   x_a, multiplying both sides by kernel function and then doing integration over the domain gives

$$\int_\Omega A(x) w(x - x_a, h) \, dx = A_a \int_\Omega w(x - x_a, h) \, dx + A_{xa} \int_\Omega (x - x_a) w(x - x_a, h) \, dx + \ldots \tag{54}$$

Ignoring derivative terms higher than first order, and writing the integral in particle approximation form leads to:

$$A_a = \frac{\sum_b m_b \frac{A_b}{\rho_b} w(x_a - x_b, h)}{\sum_b m_b \frac{1}{\rho_b} w(x_a - x_b, h)} \tag{55}$$

Equation (55) implies that $\sum_b m_b \frac{1}{\rho_b} w(x - x_b, h) = 1$, which can be viewed as the approximation form of Eq. (34). The first

15   order derivative term can be obtained in a similar way:

$$\nabla A_a = \frac{\sum_b m_b \frac{A_b - A_a}{\rho_b} \nabla_a w(x_a - x_b, h)}{\sum_b m_b \frac{x_b - x_a}{\rho_b} \nabla_a w(x_a - x_b, h)} \tag{56}$$

For problems of higher dimension, the expressions for function approximation are exactly the same as Eq. (55), even though the derivation is different. The first order derivative can be obtained by solving system of equations explicitly or numerically (Chen et al., 1999).

20   ## 3.7 Multiphase SPH

Numerical simulation of multiphase flows is usually difficult due to the existence of complex evolving interfaces between phases. This presents severe challenges to conventional Eulerian grid-based numerical methods. As we discussed in the introduction section, special algorithms to treat and track the interface between different phases is required for mesh based methods

to deal with multiphase problems. What's worse, the engulfment process during plume development makes geometry of interfaces very complicated. SPH is able to handle multiphase problems without additional numerical effort for dealing with interfaces by simply tagging particles of each phase, which makes it suitable for volcanic plume simulation. Take the governing equations adopted in our model as an example. Different phases of fluid (air and erupted material) are represented by two

5 different sets of SPH particles (or discretization points). Based on assumptions we made in section 2, only density needs to be updated respectively for each phase. The updating of density is exactly the same as Eq. (38) in spirit. Particles of phase 1 are not be counted while evaluating density of phase 2 and vice versa. Updating of density is then based on the following discretized equations.

$$< \rho_\alpha^a >= \frac{\sum m_b w_{\alpha b}(h)}{\sum \frac{m_b}{\rho_b} w_{\alpha b}(h) + \sum \frac{m_j}{\rho_j} w_{\alpha j}(h)} \tag{57}$$

$$< \rho_\alpha^{sg} >= \frac{\sum_j m_j w_{\alpha j}(h)}{\sum \frac{m_b}{\rho_b} w_{\alpha b}(h) + \sum \frac{m_j}{\rho_j} w_{\alpha j}(h)} \tag{58}$$

Where the subscript a and b represents air particles (phase 1) while i and j represents erupted material. β and α represents either erupted material or air. ρ_a^a is density of phase 1 (air). ρ_i^{sg} is density of phase 2 (erupted material). $\rho = \rho^a + \rho^{sg}$ is density of mixture of air and erupted material. By definition, the mass fraction is updated according to Eq. (59).

15 $$< \xi_\alpha >= \frac{\rho_\alpha^{sg}}{\rho_\alpha} \tag{59}$$

In areas far away from the interface, updating of density is exactly the same as that for single phase flow. For example, in the right side and left side (or blue areas) in Fig. 1, where there are only air particles, Eq. (58) evaluates to zero and total density is:

$$\rho_\alpha = \rho_\alpha^a = \frac{\sum m_b w_{\alpha b}(h)}{\sum \frac{m_b}{\rho_b} w_{\alpha b}} \tag{60}$$

20 Which is a special case of Eq. (55). For these areas occupied by only particles of phase 2 and far away from the interface, similarly, the equation for density update becomes:

$$\rho_\alpha = \rho_\alpha^{sg} = \frac{\sum m_j w_{\alpha j}(h)}{\sum \frac{m_j}{\rho_j} w_{\alpha j}} \tag{61}$$

That is to say, the same density updating equation can be applied for both phases and no additional numerical treatment needed to locate where the interface is.

25 ## 3.8 Turbulence modeling with SPH

Typically, turbulence fluctuations in a volcanic column occurs at very different length scales, ranging from millimeters up to hundreds of meters. The entrainment of air and heat transfer are dominated by such turbulent fluctuations as turbulent exchange coefficients are several magnitudes larger than corresponding physical coefficients (molecular viscosity and heat conduction
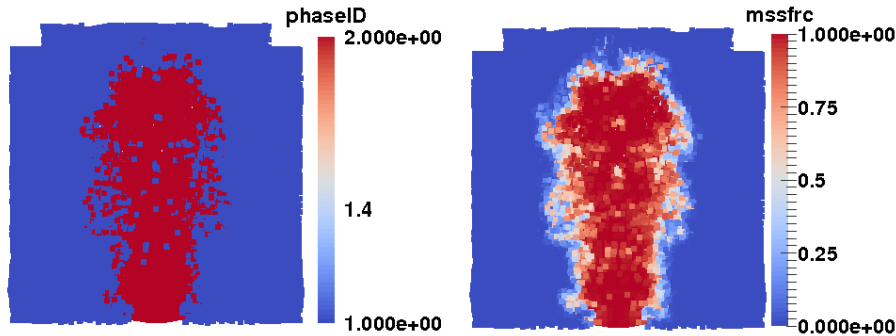
Figure 1. In the left figure, the blue particles (phaseID=1) represent air particles the red ones (phaseID=2) represent erupted material. The right figure shows corresponding mass fraction. Mass fraction are evaluated based on Eq. (57) and Eq. (57) without any other interface track or capture method.

coefficient). One way to include enough turbulence in the model is to use the SPH-SPS (SPH sub-particle-scale) turbulence model. Another way is to use fine enough resolution (namely, the direct numerical simulation method) at the expense of much higher computational cost which results from both increase in number of particles and decrease in time steps constrained by the CFL (Courant–Friedrichs–Lewy) condition. Here we choose the SPH-SPS method. Among existing SPH-SPS turbulence

5 models (Holm, 1999; Monaghan, 2002; Violeau and Issa, 2007; Monaghan, 2011), we adopt a LANS type turbulence model, the $SPH-\varepsilon$ turbulence model (Monaghan, 2011). However, the $SPH-\varepsilon$ turbulence model was proposed only for incompressible flow. In the following section, we will extend it for compressible flow. It is necessary to mention that all other existing SPH-SPS turbulence models (Holm, 1999; Monaghan, 2002; Violeau and Issa, 2007) also only focus on incompressible flow.

3.8.1 Langrangian average in $SPH-\varepsilon$

10 Monaghan (2011) constructed $SPH-\varepsilon$ turbulence model within the framework of SPH in such a way that general principles such as conservation of energy, momentum and circulation are satisfied using the ideas associated with the LANS turbulence modeling. The basic idea of $SPH-\varepsilon$ is to determine a smoothed (averaged) velocity $\widehat{\mathbf{v}}$ by a linear operation on the unsmoothed velocity $\mathbf{v}$. The SPH particles move with this smoothed velocity and hence the average motion of the fluid is determined by the averaged velocity $\widehat{\mathbf{v}}$:

$$\frac{d\mathbf{x}_a}{dt} = \widehat{\mathbf{v}}_a \tag{62}$$

Average of physical quantities over space introduces extra terms into the governing equations. Once the form of the smoothing (average) is chosen these extra terms are determined. The typical LANS model uses a smoothed velocity $\widehat{\mathbf{v}}$ defined in terms of the unsmoothed velocity $\mathbf{v}$ by:

$$\widehat{\mathbf{v}}(\mathbf{x}) = \int \mathbf{v}(\mathbf{x}\prime)\,G\left(|\mathbf{x}\prime - \mathbf{x}|, l\right) d\mathbf{x}\prime \tag{63}$$

Where G satisfies:

$$\int G\left(|\mathbf{x}\prime - \mathbf{x}|, l\right) d\mathbf{x}\prime = 1 \tag{64}$$

and is a member of a sequence of functions which tends to the δ function in the limit when $l \to 0$. A typical example is Gaussian. The length scale l determines the characteristic width of the kernel and the distance over which the velocity is smoothed.

5   It is a common practice in LANS to use a differential equation for the smoothing rather than the integral form and finally reach to a system of equations that need to be solved implicitly. In $SPH - \varepsilon$ method, a XSPH (Monaghan, 1989) smoothing is adopted which conserves linear and angular momentum. In this way, solving of a system of equations is avoided and it also makes the method simple to implement and cheap for computation. The discretized form of the momentum equation is obtained through lengthy derivation. Derivation and other discussions are available in the literature – see for e.g. (Monaghan,

10   2011). Here we provide a brief summary of key steps.

The smoothing adopted by Monaghan (2011) is:

$$\widehat{\mathbf{v}}(\mathbf{x}) = \mathbf{v}(\mathbf{x}) + \epsilon \int \left(\mathbf{v}(\mathbf{x}\prime) - \mathbf{v}(\mathbf{x})\right) G\left(|\mathbf{x}\prime - \mathbf{x}|, l\right) d\mathbf{x}\prime \tag{65}$$

As function G has the same feature as kernel function w, SPH approximation of the integration leads to:

$$\widehat{\mathbf{v}}(\mathbf{x}) = \mathbf{v}(\mathbf{x}) + \epsilon \sum_b m_b \frac{(\mathbf{v}_b - \mathbf{v})}{\rho_b} G\left(|\mathbf{x}_b - \mathbf{x}|, l\right) \tag{66}$$

15   By making the replacement:

$$\frac{G\left(|\mathbf{x}_b - \mathbf{x}_a|, l\right)}{\rho_b} \to \frac{K_{ab}}{M} \tag{67}$$

Where $K_{ab} = l^d G_{ab}$, $M = \rho_0 l^d$ in which d is the dimension and ρ_0 is initial density. $SPH - \varepsilon$ turbulence model is obtained after lengthy derivation:

$$\frac{d\mathbf{v}_a}{dt} = -\sum_b \left[m_b \left(\frac{p_b}{\rho_b^2} + \frac{p_a}{\rho_a^2}\right) \bigtriangledown_a w_{ab}(h)\right] + \sum_b m_b \frac{\varepsilon}{2} \frac{\mathbf{v}_{ab} \cdot \mathbf{v}_{ab}}{M} \bigtriangledown_a K_{ab} \tag{68}$$

20   Notice that if l is ~~uniform~~:

$$\nabla K_{ab} = \nabla \left(l^d G_{ab}\right) = l^d \nabla G_{ab} \tag{69}$$

The discretized momentum equation with $SPH - \varepsilon$ turbulence model can be written in terms of G_{ab} instead of K_{ab}:

$$\frac{d\mathbf{v}_a}{dt} = -\sum_b \left[m_b \left(\frac{p_b}{\rho_b^2} + \frac{p_a}{\rho_a^2}\right) \bigtriangledown_a w_{ab}(h)\right] + \sum_b m_b \Phi_{ab} \bigtriangledown_a G_{ab}(l) \tag{70}$$

where

25    $$\Phi_{ab} = \frac{\varepsilon}{2} \frac{\mathbf{v}_{ab} \cdot \mathbf{v}_{ab}}{\rho_b} \tag{71}$$

Which is the extra stress term induced by average. We take coefficient ε as 0.8 following Monaghan (2011).

For compressible flow, the energy equation is coupled with the momentum equation and mass conservation equation. Averaging of thermal energy over space introduces some additional terms besides the stress term induced by velocity average. (Rumsey, 2014). The averaged momentum equation for compressible flow are in the same form as that for incompressible flow, all of other additional terms, besides the corresponding velocity average induced stress term, show up in the energy

5   equation. Most turbulence modeling focuses on the stress terms induced by average of velocity. These stress terms are usually either solved directly (for example, LANS methods) or defined via a constitutive relation (for example, large eddy simulation method). Less attention is typically given to the other terms. Most commonly, a Reynolds analogy is used to model the turbulent exchange. Simulations of heat transfer, or other scalar transfer, in turbulent flow simply involve adding transport terms for thermal energy or species concentration, at the expense of greater storage and longer computing times but without other diffi-

10   culties (Cebeci, 2013). We adopt this strategy. The additional terms associated with molecular diffusion and turbulent transport in the energy equation are either modeled in different ways or neglected sometimes (Rumsey, 2014). We neglect these terms in our simulation.

3.8.2   Turbulent heat transfer

We adopt Reynolds analogy to get the heat transfer coefficient due to turbulence. The Prandtl number is defined as:

$$Pr = \frac{C_p \mu}{\kappa} \tag{72}$$

Where, μ is the dynamic viscosity, κ is the thermal conductivity. And μ can be written in term of the absolute viscosity (kinematic viscosity) as:

$$\mu = \rho \nu \tag{73}$$

Then

$$\kappa = \frac{C_p \mu}{Pr} \tag{74}$$

Typical value of Pr_t for air is $0.7 \sim 0.9$. We take $Pr_t = 0.85$ for gases as recommended Kays (1994) from summarizing of experimental results.

Monaghan (2005) summarized the simulation of viscosity and heat conduction in his review on SPH. We will refer to his summary in our following discussion. The additional term in discretized momentum equation, Eq. (70), is the turbulent shear

25   stress term. Recall that molecular viscosity can be discretized with SPH as shown in Eq. (45). It has been shown that the discretized molecular viscosity has both bulk viscosity and shear viscosity, where shear viscosity coefficient is (Monaghan, 2005):

$$\nu_t = S\nu \tag{75}$$

with

$$S = \begin{cases} \dfrac{1}{10} & if \quad d = 3 \\[2em] \dfrac{1}{8} & if \quad d = 2 \end{cases} \tag{76}$$

The turbulent viscosity coefficient can be inferred from that formulation if we can reformulate the turbulent shear stress term in a form which is similar to the molecular shear term. Reformulate the turbulent shear stress term:

$$\sum_b \frac{\varepsilon}{2} \frac{m_b}{\rho_b} \mathbf{v}_{ab} \cdot \mathbf{v}_{ab} \nabla_a G_{ab}(l_a) = \sum_b \frac{\varepsilon}{2S} m_b \frac{\mathbf{v}_{ab}}{\rho_b} \frac{S\mathbf{v}_{ab} \cdot \mathbf{x}_{ab}}{x_{ab}^2} \frac{x_{ab}^2}{\mathbf{x}_{ab}} \nabla_a G_{ab}(l_a) \tag{77}$$

Then the turbulent viscosity coefficient can be inferred from Eq. (77).

$$\nu_t = \frac{\varepsilon}{2S} \frac{\mathbf{v}_{ab} \cdot \mathbf{x}_{ab}}{\rho_b} \tag{78}$$

Please note that turbulent viscosity term has opposite sign with molecular viscosity term in discretized momentum equation and there is a minus sign in the expression of Π_{ab}, and they cancel out.

However, the above equation is correct only for the 1D situation. For 2D or 3D, it is not easy to get an explicit expression. We adopt an alternative way: obtaining a value for each pair of particles instead of persisting on getting an analytical expression. Choosing the smoothing function as the same as SPH kernel and the smoothing length scale l as the same as smoothing length h, the ratio between turbulent shear stress and physical shear stress is:

$$\begin{aligned} \Upsilon_{ab} &= \frac{\dfrac{\varepsilon}{2} \dfrac{\mathbf{v}_{ab} \cdot \mathbf{v}_{ab}}{\rho_b}}{\dfrac{S\nu}{\rho_{ab}} \dfrac{\mathbf{v}_{ab} \cdot \mathbf{x}_{ab}}{x_{ab}^2 + \eta^2 h_{ab}^2}} \\ &= \frac{\varepsilon \left(x_{ab}^2 + \eta^2 h_{ab}^2 \right)}{2S\nu} \frac{\mathbf{v}_{ab} \cdot \mathbf{v}_{ab}}{\mathbf{v}_{ab} \cdot \mathbf{x}_{ab}} \end{aligned} \tag{79}$$

Υ_{ab} is essentially equivalent to the ratio between turbulent viscous effect of particle b on particle a and molecular viscous effect of particle b on particle a. Turbulent viscosity can be easily obtained by:

$$\begin{aligned} \nu_{t,ab} &= \nu \Upsilon_{ab} \\ &= \frac{\varepsilon \left(x_{ab}^2 + \eta^2 h_{ab}^2 \right)}{2S} \frac{\mathbf{v}_{ab} \cdot \mathbf{v}_{ab}}{\mathbf{v}_{ab} \cdot \mathbf{x}_{ab}} \end{aligned} \tag{80}$$

The corresponding turbulent thermal conductivity should be

$$\kappa_{t,ab} = \frac{\varepsilon \overline{C_{p,ab}} \, \overline{\rho_{ab}} \left(x_{ab}^2 + \eta^2 h_{ab}^2 \right) \mathbf{v}_{ab} \cdot \mathbf{v}_{ab}}{2S Pr_t \mathbf{v}_{ab} \cdot \mathbf{x}_{ab}} \tag{81}$$

$\overline{C_{p,ab}}$ and $\overline{\rho_{ab}}$ are simply the arithmetic means of specific heat and density. The term used to prevent singularity now can be removed.

$$\kappa_{t,ab} = \frac{\varepsilon \overline{C_{p,ab}} \, \overline{\rho_{ab}} \, x_{ab}^2 \mathbf{v}_{ab} \cdot \mathbf{v}_{ab}}{2S Pr_t \mathbf{v}_{ab} \cdot \mathbf{x}_{ab}} \tag{82}$$

We also need to prevent singularity, so:

$$\kappa_{t,ab} = \begin{cases} 0 & if \quad \mathbf{v}_{ab} = 0 \quad or \quad \mathbf{x}_{ab} = 0 \\ \dfrac{\varepsilon \overline{C_{p,ab}}\,\overline{\rho_{ab}}\, x_{ab}^2 \mathbf{v}_{ab} \cdot \mathbf{v}_{ab}}{2 S Pr_t \mathbf{v}_{ab} \cdot \mathbf{x}_{ab}} & \text{otherwise} \end{cases} \tag{83}$$

Heat conduction equation without source term is:

$$C_p \frac{dT}{dt} = \frac{1}{\rho} \nabla (\kappa \nabla T) \tag{84}$$

Second spatial derivative can be approximated with SPH by following Monaghan (2005):

$$C_p \frac{dT}{dt} = \sum_b \frac{m_b}{\rho_a \rho_b} (\kappa_a + \kappa_b)(T_a - T_b) F_{ab}(h) \tag{85}$$

Where

$$F_{ab}\mathbf{x}_{ab} = \nabla_a w_{ab} \tag{86}$$

F_{ab} is nonpositive, which guarantees that heat flux flows from hot to cold. Plug the turbulent thermal conductivity into the heat conduction equation:

$$C_p \frac{dT}{dt} = \sum_b \frac{m_b}{\rho_a \rho_b} (\kappa_a + \kappa_b)(T_a - T_b) F_{ab}(h)$$
$$= 2 \sum_b \frac{m_b}{\rho_a \rho_b} \frac{\overline{C_{p,ab}}\,\overline{\rho_{ab}}\varepsilon x_{ab}^2 \mathbf{v}_{ab} \cdot \mathbf{v}_{ab}}{2 Pr_t S \mathbf{v}_{ab} \cdot \mathbf{x}_{ab}} (T_a - T_b) F_{ab}(h) \tag{87}$$

Notice that the number "2" in the front of Eq. (87) comes from integration approximation of second order derivative (Cleary and Monaghan, 1999). By further simplification, we get:

$$C_p \frac{dT}{dt} = \frac{\varepsilon}{S Pr_t} \sum_b \frac{m_b}{\rho_a \rho_b} \frac{\overline{C_{p,ab}}\,\overline{\rho_{ab}} x_{ab}^2 \mathbf{v}_{ab} \cdot \mathbf{v}_{ab}}{\mathbf{v}_{ab} \cdot \mathbf{x}_{ab}} (T_a - T_b) F_{ab}(h) \tag{88}$$

3.8.3 Discretized governing equations with $SPH - \varepsilon$ turbulence model

Plugging in the discretized turbulent stress term and turbulent heat transfer term into the momentum and energy equation, we get new discretized governing equations:

$$\left\langle \frac{d\mathbf{v}_\alpha}{dt} \right\rangle = -\sum_b \left[m_b \left(\frac{p_b}{\rho_b^2} + \frac{p_\alpha}{\rho_\alpha^2} + \Pi_{\alpha b}^\beta - \Phi_{\alpha b} \right) \nabla_\alpha w_{\alpha b}(h) \right] - \sum_j \left[m_j \left(\frac{p_j}{\rho_j^2} + \frac{p_\alpha}{\rho_\alpha^2} + \Pi_{\alpha j}^\beta - \Phi_{\alpha j} \right) \nabla_\alpha w_{\alpha j}(h) \right] + \mathbf{g} \tag{89}$$

With

$$\Phi_{\alpha\beta} = \frac{\varepsilon}{2} \frac{\mathbf{v}_{\alpha\beta} \cdot \mathbf{v}_{\alpha\beta}}{\rho_\beta} \tag{90}$$

$$\left\langle \frac{de_\alpha}{dt} \right\rangle = 0.5 \sum_b \left[m_b \widehat{\mathbf{v}_{\alpha b}} \left(\frac{p_b}{\rho_b^2} + \frac{p_\alpha}{\rho_\alpha^2} + \Pi_{\alpha b}^\beta - \Phi_{\alpha b} \right) \bigtriangledown_\alpha w_{\alpha b}(h) \right] + 2 \sum_b \frac{m_b}{\rho_\alpha \rho_b} \kappa_{t,\alpha b}(T_\alpha - T_b) F_{\alpha b}(h)$$

$$+ 0.5 \sum_j \left[m_j \widehat{\mathbf{v}_{\alpha b}} \left(\frac{p_j}{\rho_j^2} + \frac{p_\alpha}{\rho_\alpha^2} + \Pi_{\alpha j}^\beta - \Phi_{\alpha j} \right) \bigtriangledown_\alpha w_{\alpha j}(h) \right] + 2 \sum_j \frac{m_j}{\rho_\alpha \rho_j} \kappa_{t,\alpha j}(T_\alpha - T_j) F_{\alpha j}(h) \tag{91}$$

with $\kappa_{t,\alpha\beta}$ given by Eq. (83). As the particle-scale movement of flow is based on smoothed velocity, the velocity in the energy equation should also be smoothed. The filtering process is done according to Eq. (66). Position of particles is updated according to Eq. (62). Smoothed velocity is also used while computing artificial viscosity.

3.9 Boundary conditions

All boundary conditions are imposed by ghost particles. Subfigure b of Fig. 2 shows how boundaries are deployed.

3.9.1 Wall boundary condition

Traditionally either ghost particles that mirror real particles across the boundary (Ferrari et al., 2009) or boundary forces (Monaghan and Kajtar, 2009) have been used to impose the wall boundary conditions. One disadvantage of the latter is that the boundary forces tend to corrupt the solution in the local neighborhood. In addition, a natural way of imposing eruption boundary condition is using eruption ghost particles. To impose boundary conditions in a consistent way, we adopt a modified version of the ghost particle method (Kumar et al., 2013) for wall boundary conditions. Stationary wall ghost particles are deployed in the same way as real particles. Instead of enforcing symmetry particle by particle, a symmetric field across the boundary is explicitly enforced. Ghost particles are reflected into the domain and physical quantities are calculated at these reflected positions by SPH interpolations. It should be noted that wall ghost particles should not be counted when computing physical properties of these reflected positions. Assign all properties, except for velocity, at the corresponding reflected position to the ghost particle. The velocity of each wall ghost particles is set to have the same value but opposite direction of the interpolated velocity at its corresponding reflection. By this way, the no-slip wall boundary condition (Eq. (22)) is imposed naturally. These wall ghost particles serve as neighbors in momentum and energy update. More implementation details about this method can be found in (Kumar et al., 2013). As these wall ghost particles are stationary, there is no mass flux on the boundary (Eq. (20) and (21)). In addition, as temperature is also symmetric with respect to the boundary, the gradient of temperature vanishes and hence there is no internal energy flux on the wall boundary (Eq. (23)).

3.9.2 Eruption boundary condition

A natural way of imposing eruption boundary condition is using ghost particles that move with the eruption velocity and bear the temperature of the erupted material. A parabolic velocity profile that represents a fully developed Hagen-Poiseuille flow is used to determine the inlet particle velocity. The detailed shape of the parabolic profile is determined based on an averaged eruption velocity (Eq. (18)). The mass of eruption ghost particles is set to a value so that evaluation of Eq. (38) can return

us a density that is consistent with the value given in Eq. (16). The internal energy associated with these particles are set to a value so that Eq. (19) is satisfied. The mass fraction of erupted material (Eq. (17)) is automatically satisfied as all particles in the eruption conduit are of phase 2. The density, momentum, and internal energy of these eruption ghost particles are not updated before they move above ground. As soon as they move out from erupt conduit, these ghost particles will be shifted to

5   real particles and their physical quantities and position will be updated based on discretized governing equations. New ghost particles need to be added at the bottom of the eruption conduit as these existing ghost particles move upwards.

3.9.3 Pressure boundary condition

Another boundary condition in our model is the pressure outlet boundary. For flow in a straight channel, it is possible to treat the exit the same as the entry with a prescribed velocity profile. For flow with more complex channel, an exit far downstream of

10   the flow disturbance is also feasible. However, the natural boundary condition (Eq. (24)) is more suitable for plume simulation as the outlet is open atmosphere. The way we impose pressure boundary condition is: adding several layers of pressure ghost particles surrounding the real atmosphere particles. Pressure, density and temperature are determined based on the elevation of particles. Velocity is set to zero for static atmosphere. The physical quantities for pressure ghost particles are not updated while these for real particles are updated at every time step. As position of all pressure ghost particles keep constant, we essentially

15   impose a static pressure boundary condition. Real particles removed as soon as they move out the pressure boundary.

As simulations progress, changes in position and physical quantities of real particles near pressure boundaries might corrupt pressure boundary condition that was established initially. This shortcoming is relieved by choosing a larger computational domain so that boundaries that might be corrupted locate far away from turbulent mixing area. In addition, to avoid enlarging fluctuations, we add another constraint on the time step:

20   $$\Delta t \leq CFL_p \frac{h}{v} \tag{92}$$

Where CFL_p is a safety coefficient which has similar function as the normal CFL number. Too small CFL_p would slow down simulation while too large CFL_p would lose its ability of mitigate numerical fluctuation near the boundary. The proper CFL_p is determined by series of simulation tests.

3.10 Parallellism and performance

25   One disadvantage of the 3D model is that it usually takes a much longer time than 1D models to complete one simulation. This disadvantage further prevents doing simulation with finer resolution and accounting for more physics in one model. Non-intrusive uncertainty analysis, which is commonly adopted in hazard forecasting, requires finishing multiple simulations within a given time window. High performance computing is therefore essential. Among existing CPU parallel SPH schemes, most of them focus on neighbor searching algorithm and dynamic load balancing (eg. Ferrari et al., 2009; Crespo et al., 2015).

30   Less attention has been paid to developing more flexible data management schemes for more complicated problems. Motivated by techniques developed for mesh based methods, we develop a complete framework for parallelizing SPH with distrubted memory parallelism (MPI) allowing flexible and efficient data access.
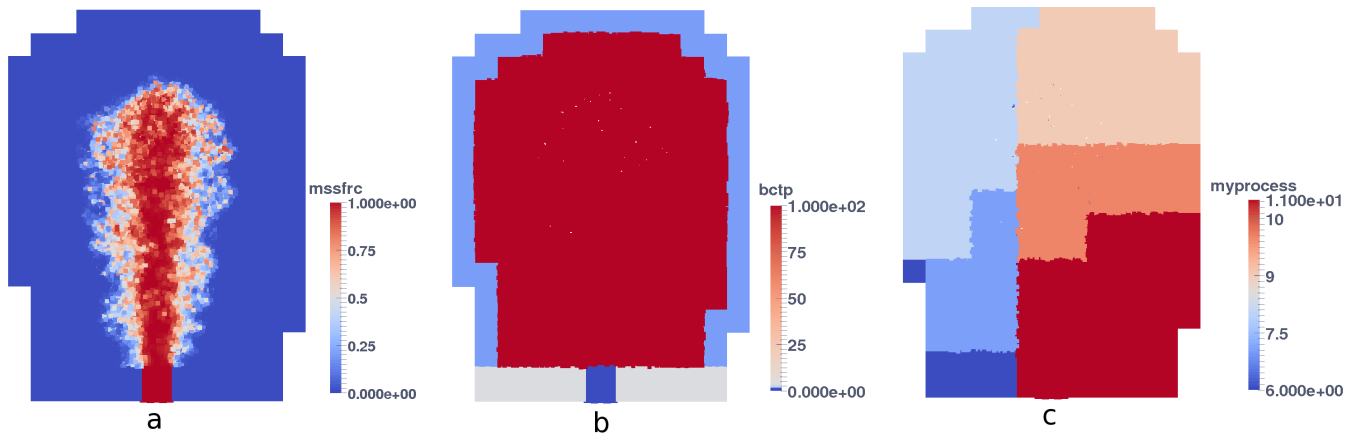
Figure 2. A cross section view of the simulation domain in $y-z$ plane at 66 seconds. Subfigure a shows the mass fraction. Subfigure b shows all boundary conditions: the dark blue region are occupied by eruption ghost particles with "Ghost particle ID" of 0, the light blue area are occupied by pressure ghost particles with "Ghost particle ID" of 1, the gray area is filled with wall ghost particles with "Ghost particle ID" of 2, "Ghost particle ID" of all real particles are set to 100, they occupy the major portion of the domain in subfigure b. Subfigure c shows the cross section view of domain decomposition based on SFC. The simulation is conducted on 12 processors, so there are 12 subdomains in total. The crosss section view shows a portion of them.

Any implementation of SPH code requires efficient searching and updating of neighbors during simulation. Of the many possible choices we adopt a background grid which was proposed by Monaghan and Lattanzio (1985) and is quite popular in parallel SPH. This background grid is also used for domain decomposition in SPH. We refer to the elements of background grid, namely squares for two dimensions and cubic for three dimensions, as buckets. As for the actual storage of the physical quantities associated to each particle, different strategies have been adopted in existing implementations of SPH.

5   In DualSPHysics (Crespo et al., 2015), the physical quantities of each particle (position, velocity, density...) are stored in arrays. The particles (and the arrays with particle data) are reordered following the order of the cells. This has two advantages: 1) access pattern is more regular and more efficient, 2) it is easy to identify the particles that belong to a cell by using a range since the first particle of each cell is known. But adding, deleting and especially accessing of particles are cumbersome.

10   Ferrari et al. (2009) adopted linked lists using pointers so that particles can be deleted or added during the simulation. Storage problems caused by fixed-size arrays are thereby also eliminated. We define C++ classes which contain all data of particles and buckets. As for the management of data, we adopt hash tables to store pointers to particles and buckets, which gives us not only flexibility of deleting and adding of elements, but also quicker access compared with linked lists. Instead of using the "nature manner" to number particles, we adopt a space filling curve (SFC) based index to give each particle and background

15   bucket an unique identifier – a strategy known to preserve data locality at minimal cost. The SFC based numbering strategy is further extended to include time step information so that particles added at the same position but different time have different identifiers.
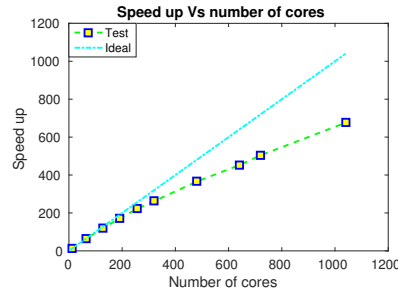
Figure 3. Strong scalability test result
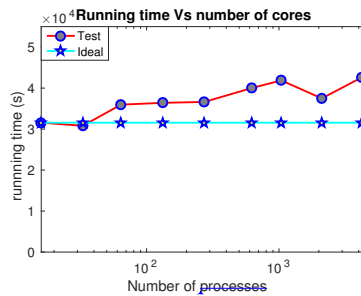
Figure 4. Weak scalability test result
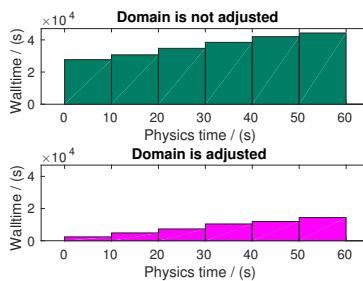
Figure 5. The effect of domain adjusting on simulation time. The figure on the top shows execution time without domain adjusting, the figure on the bottom shows execution time with domain adjusting. Different bins represent execution time up to specific physical time indicated by horizontal axis.

As for domain decomposition, even though more complicated graph-based partitioning tools (Biswas and Oliker, 1999) might get higher quality decomposition, they requires much more effort in programming and computation. So we adopt an easy-programming scheme based on SFC (Patra and Kim, 1999). Subfigure c of Fig. 2 shows a cross section view of domain decomposition.

5   More details about the data structure, domain decomposition, load balancing and domain adjusting will be published separately.

Performance tests have been carried out on the computational cluster of CCR (Center for Computational Research) at Buffalo. Intel Xeon E5645 CPUs running at 2.40GHz clock rate with 4GB memory per core on a Q-Logic Infiniband is used in these tests. Each node is comprised of two sockets with 6 of these cores. Memory and level 3 cache are shared on each node. The initial domain is $[-4.8km, 4.8km] \times [-4.8km, 4.8km] \times [0km, 6km]$. Almost linear speed up is observed in our
5 strong scalability test (Fig. 3).

The weak scalability test is conducted with the same initial domain and various smoothing lengths. Each simulation runs for 400 time steps. The average number of real particles of each process keeps constant at 25900. As shown in Fig. 4, simulation times increase around $1/3$ when number of cores increase from 16 to 4208. For the test problem in this section, the volcanic plume finally reaches to a region of $[-30km, 30km] \times [-30km, 30km] \times [1.5km, 40km]$ after around 400 seconds of eruption.
10 When numerical simulation goes up to 90 seconds, the plume is still within a region of $[-10km, 10km] \times [-10km, 10km] \times [0km, 25km]$. This implies that adjusting of domain can avoid computing large number of uninfluenced air particles, especially for the beginning stage of simulation. A domain adjusting algorithm is designed and implemented in our code. Figure 5 shows that simulation time of the test problem is greatly reduced when we adopt the domain adjusting strategy.

4 Verification and validation

15 We present a series of numerical simulations to ~~verify and~~ validate our model in this section. Plume-SPH is first ~~verified~~ by a JPUE (jet or plume that is ejected from a nozzle into a uniform environment) simulation. Velocity and mass fraction distribution both along the central axis and cross transverse are compared with experimental results. The pattern of ambient particles entrainment is also clearly shown. Then a simulation of representative strong volcanic plume is conducted. Both global variables and local variable are comparable with simulation results from existing 3D plume models.

20 ### 4.1 Simulation of JPUE

JPUE can be considered as a simplified volcanic plume. While the effect of stratified atmosphere and the effect of expansion due to high temperature in volcanic plume are not represented, JPUE reproduces the entrainment due to turbulent mixing which is one of the key elements in volcanic plume development. There exist consistently good experimental data (List, 1982; Dimotakis et al., 1983; Papanicolaou and List, 1988) that describe the JPUE flow field giving an insight into details of JPUE,
25 such as transverse velocity and concentration profile. In this section, we verify that our code and the $SPH - \varepsilon$ turbulence model is able to reproduce feature of turbulent entrainment by a JPUE simulation.

As many of these experiments were conducted with liquid, we replace the original equation of state (Eq. (5)) with a weakly compressible Tait equation of state (Becker and Teschner, 2007) (see Eq. (93)) to avoid solving the Poisson equation.

$$p = B \left[\left(\frac{\rho}{\rho_0} \right)^{\gamma} - 1 \right] \tag{93}$$

30 with $\gamma = 7$ and B is evaluated by:

$$B = \frac{\rho_0 c^2}{\gamma} \tag{94}$$
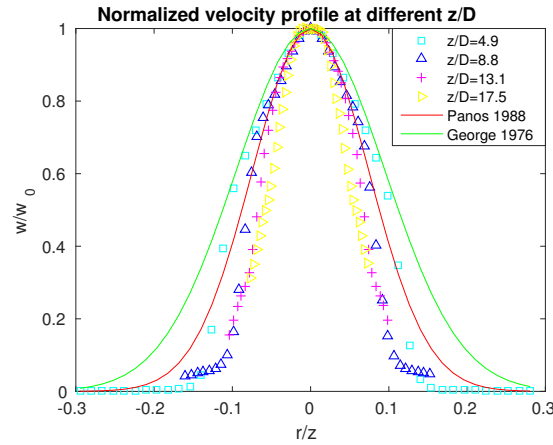
Figure 6. Dimensionless velocity distribution across the cross-section.

Where c is the speed of sound in the liquid. The energy equation is actually decoupled from the momentum conservation equation and the mass conservation equation by using this equation of state (EOS). In addition, the "atmosphere" is assumed to be uniform and gravity is set to be zero. We set the temperature and density of ejected material the same as surrounding ambient. This further simplifies the scenario for the convenience of studying turbulent mixing.

5   One overall feature of JPUE is "self-similarity" which means that the evolution of the JPUE is determined solely by the local scale of length and velocity which theoretically account for the fact that the rate of entrainment at the edge of JPUE is proportional to a characteristic velocity at each height. As a results, physical and numerical experiments do not necessary to have exactly the same setups and are compared on a non-dimensional basis.

Table 1. List of eruption condition for the test cases

Parameters	Units	JPUE	Plume
Vent velocity	$m \cdot s^{-1}$	500	275
Vent gas mass fraction		1.0	0.5
Vent Temperature	K	273	1053
Vent height	m	0	1500
Mass discharge rate	$kg \cdot s^{-1}$	5.47×10^7	1.5×10^9

    A three dimensional axisymmetric JPUE which ejects from a round vent is simulated with eruption parameters listed in
10   Table 1. Material properties of water are used as material properties for both phases. The results are compared with experiments (George et al., 1977; Papanicolaou and List, 1988) for validation purposes. Experimental data of concentration and velocity distribution across the cross-section were fit into a Gaussian profile: $\frac{\varphi}{\varphi_c} = exp\left[-coef\left(\left(\frac{r}{z}\right)^2\right)\right]$ (solid line) by Papanicolaou and List (1988) even though the actual profile are slightly different from the Gaussian profile. Papanicolaou and List (1988) also fit concentration distribution and jet width based on velocity along central line into a straight line :
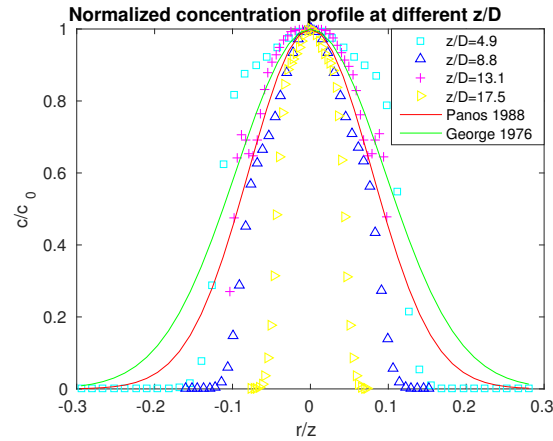
Figure 7. Dimensionless concentration distribution across the cross-section.
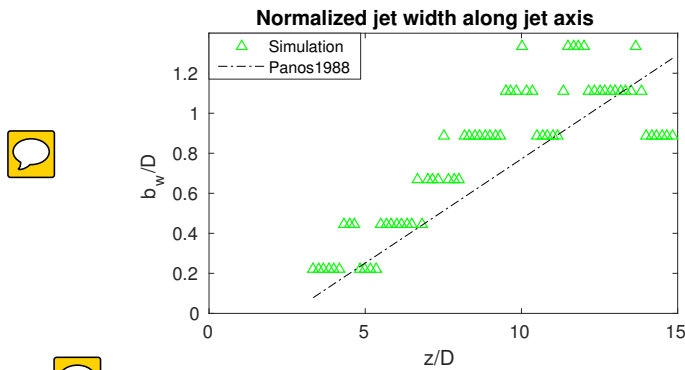
Figure 8. Dimensionless velocity distribution along centraline.
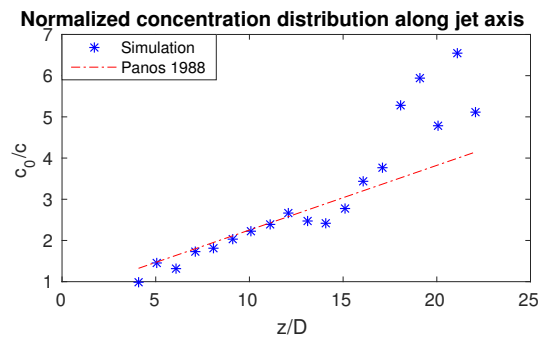
Figure 9. Dimensionless concetration distribution along centraline.
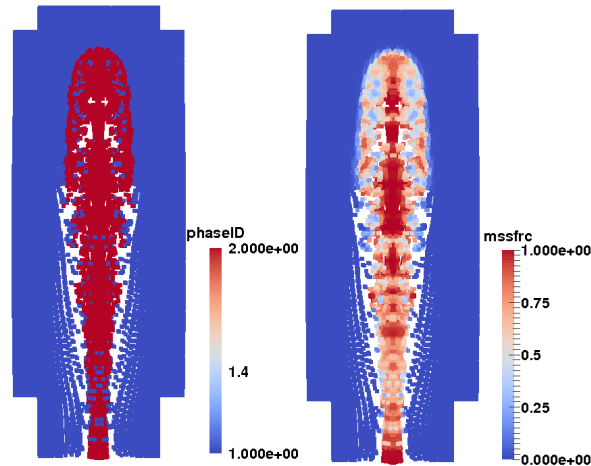
Figure 10. The left figure shows particle distribution. Particles of phase 1 (blue) are gradually entrained and mixed with erupted particles (red) as jet flows down stream. The right figure shows the mass fraction of erupted material at the moment corresponding to the left figure.

$\dfrac{\varphi_0}{\varphi_c} = slope \left(\dfrac{z}{D} + intercept \right)$ (dash line). φ is either velocity or concentration, the subscript c represents the centreline, subscript 0 represents the cross-sectionally averaged exit value. r is the distance from the centreline on any cross-section. z is the axial distance from the origin of the jet transverse section under consideration. D is the diameter of vent. The coefficient $coef$ for concentration is 80 and 50 respectively according to George et al. (1977) and Papanicolaou and List (1988). $coef$ for velocity is 90 and 55 respectively according to George et al. (1977) and Papanicolaou and List (1988). $slope$ for jet width based on velocity is 0.104 and for concentration is 0.157. $intercept$ for jet width based on velocity is 2.58 while that for the concentration is 4.35.

Although both velocity and concentration are found to be well matched with experimental results, a small disparity in both velocity and concentration are observed near the boundary of the jet. There are several factors that would attribute to such disparity. Reynolds number is not reported in many experiments assuming a high enough Reynolds number. In addition, some details of the experiments, such as exit velocity profile and viscosity of the experimental liquid, are not reported. These factors prevent us from numerically reproducing these experiments in an exact way as they were conducted. However, the features of JPUE is correctly reproduced with our code.

We also investigated the mixing due to turbulence in JPUE simulation by checking the mixture of the two phases. It is shown in Fig. 10 that the ejected material and ambient fluids are mixed through eddies at the outer shear region. And the inner dense core dispersed gradually due to erosion of the outer shear region. Hence, our confidence in the numerical correctness of our code is greatly reinforced.

4.2 Simulation of a plume

The development of a volcanic plume is more complicated than JPUE in several aspects. Besides turbulent entrainment of ambient fluids, development of volcanic plume also involves heating up of entrained air and expanding in a stratified atmosphere. A strong eruption column without wind is tested in this section for the purpose of further verification and validation. Both
5   global variable and local variables are compared with existing models.

4.2.1 Input parameters

Eruption parameters, material properties and atmosphere are chosen to be the same as the strong plume no wind case in a comparison study on eruptive column models (Costa et al., 2016). Eruption conditions are listed in Table 1. The density of erupted material at the vent and radius of the vent can be computed from the given parameters. The eruption pressure is assumed
10   to be as the same as pressure of ambient at the vent and hence is not given in the table. The vertical profiles of atmospheric properties were obtained based on the reanalysis data from ECMWF (European Centre for Medium-Range Weather Forecasts) for the period corresponding to the climactic phase of the Pinatubo eruption (Philippines, 15 June 1991). These conditions are more typical of a tropical atmosphere (see Fig. 1B in (Costa et al., 2016)). Vertical distribution of temperature, pressure and density is used to establish stratified atmosphere. Material properties, shown in Table 2, are selected based on properties
15   of Pinatubo and Shinmoe-dake eruption. Other material properties not given in the table can be infered from these given parameters based on their relationships.

Table 2. List of material properties

Parameters	Units	Value
Specific heat of gas at constant volume	$J \cdot kg^{-1} \cdot K^{-1}$	717
Specific heat of air at constant volume	$J \cdot kg^{-1} \cdot K^{-1}$	1340
Specific heat of solid	$J \cdot kg^{-1} \cdot K^{-1}$	1100
Specific heat of gas at constant pressure	$J \cdot kg^{-1} \cdot K^{-1}$	1000
Specific heat of air at constant pressure	$J \cdot kg^{-1} \cdot K^{-1}$	1810
Density of air at vent height	$kg \cdot m^{-3}$	1.104
Pressure at vent height	Pa	84363.4

4.2.2 Global and local variables

One of the key global quantities of great interest is the altitude to which the plume rises. The top height predicted by our model is around 40 km which agrees with other plume models. For example, the height predicted by PDAC is 42500 m, by SK-3D is
20   39920 m, by ATHAM is 33392 m, by AHSEE is 36700 m. As for local variables, the profiles of integrated temperature, density, mass fraction of entrained air, gas mass fraction, mass fraction of solid and the radius of the plume as a function of height are compared with existing 3D models in Fig. 11 ~ 14. To get rid of significant fluctuations in time and space we conducted a time
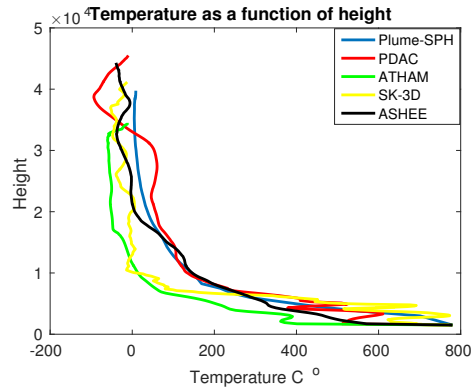
Figure 11. Temperature as a function of height
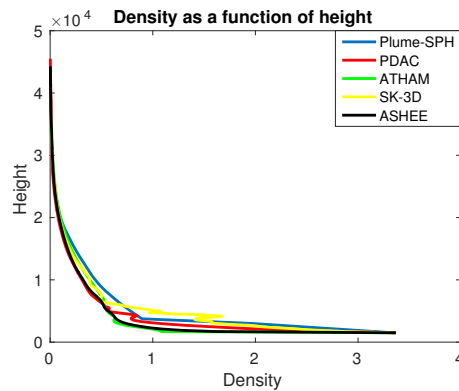
Figure 12. Density of the strong plume without wind after reaching its top height

averaging and spatial integration of the dynamic 3D flow fields by following Cerminara et al. (2016b). As particles distribute in a disordered manner in the space in SPH simulation results. We first project simulation results (on disordered particles) onto a pre-defined grid before doing time average and spatial integration. The project method is the basic SPH kernel based interpolation.

5 The profiles of local variables match well with simulation results of existing 3D models in a general sense. The basic phenomena in volcanic plume development is correctly captured by our model.

As the height increases, the amount of entrained air also increases. Around the neutral height, where the umbrella expands, the entrainment of air shows a slight decrease due to lack of air surrounding the column at that height. The profile for gas, which account for both air and vapor, shows a very similar tendency as that of entrained air. Recall that vapor condensation

10 is not considered in our model. In addition, we assume that erupted material behaves like a single phase fluid. So the mass fraction of gas is simply a function of entrained air (Eq. (95)). Among these 3D models, ATHAM takes vapor condensation into account and Eq. (95) does not hold for ATHAM. However, the profile of entrained air and profile of gas predicted by ATHAM
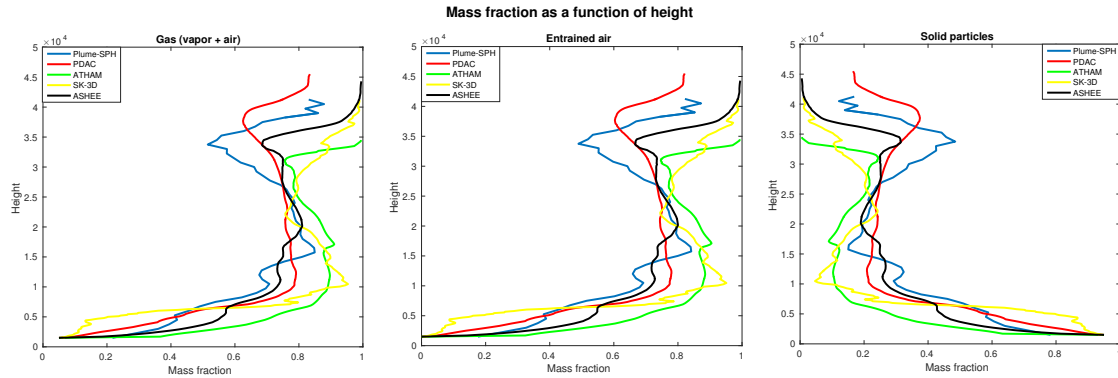
Figure 13. The mass fraction of entrained air, gas, and solid as a function of height.
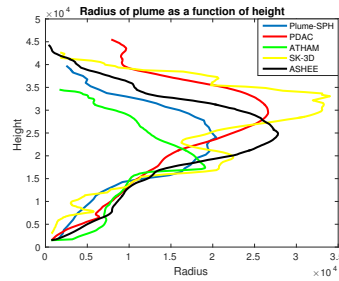
Figure 14. Radius of the strong plume without wind after reaching its top height.

are still very close to each other which implies that ignoring of water phase change is a valid assumption for eruptions similar to this test case (strong plume with erupted water fraction in erupted material less than 5%). This observation can be explained by the fact that air occupies a larger portion of the gas and ignoring of phase change of vapor (which is only a small portion of gas) causes slight influence on plume development. As for mass fraction of solid, similarly, Eq. (96) and Eq. (97) hold for

5   our model. PDAC, which treat particles of two different sizes as two separate phases, predicted a similar mass fraction profile. That implies that assumption of dynamic equilibrium in our model is at least valid for eruptions similar to the test case.

$$\xi_a + \xi_g = \xi_a + (1 - \xi_a)\xi_{g0} \tag{95}$$

$$\xi_s = (1 - \xi_a)(1 - \xi_{g0}) \tag{96}$$

$$\xi_s = 1 - (\xi_a + \xi_g) \tag{97}$$

With more cool air entrained into the plume and mixing with the hot erupted material, the temperature of the plume decreases as the height increases as shown in Fig. 11. In the meanwhile, bulk density decrease due to entrainment and expansion (Fig. 12).

Our model adopts the same assumptions and governing equations as SK-3D. However, there is still a big disparity between the profiles of local variables of our model and SK-3D. One of the big differences between these two models is that we adopt a LANS type of turbulence model while SK-3D adopts a LES (large eddy simulation) turbulence model. This implies that turbulence model might play a critical role in plume simulation.

5 Conclusions

A new plume model was developed based on the SPH method. Extensions necessary for Lagrangian methodology and compressible flow were made in the formulation of the equations of motion and turbulence models. Advanced numerical techniques in SPH were exploited and tailored for this model. High performance computing was used to mitigate the tradeoff between accuracy (depends on comprehensiveness of the model, resolution, order of accuracy of numerical methods, scheme for time upgrading.) and simulation time (depends on comprehensiveness of model, resolution, order of accuracy of numerical methods, scheme for time upgrading ... and computational techniques). The correctness of the code and model was verified and validated by a series of test simulations. Dimensionless velocity and concentration distribution across the cross-section and along the jet axis match well with experimental results of JPUE. Top height and integrated local variables simulated by our model are consistent with simulation results of existing 3D plume models. Comparison between our results with these of SK-3D implies that turbulence model plays a significant role in plume modeling.

Currently existing 3D models focus on certain aspect of the volcanic plume (PDAC on pyroclastic flow, ATHAM on microphysics, and SK-3D on entrainment with higher accuracy and higher order of accuracy) and hence, naturally, different assumptions were made in these models. However, these different aspects of volcanic plumes are not independent, but are actually coupled. For example, it has been illustrated by Cerminara et al. (2016b) that gas-particle non-equilibrium would introduce a previously unrecognized jet-dragging effect, which imposes great influence on plume development, especially for weak plumes. In addition, there is no absolute boundary to determine which kind of hazard is dominant in certain eruptions. So it is necessary to simulate all associated hazards in one model. Actually, effort has already been put on developing more comprehensive plume models. For example, a large-particle module (LPM) was added to ATHAM to track the paths of rocky particles (pyroclastic or tephra) within the plume and predict where these particles fall (Kobs, 2009). We were also motivated by such an evolution of plume modeling to choose SPH as our numerical tool. Besides its ability in dealing with interfaces for multiphase flows, as mentioned in the introduction section, SPH method has good extensibility and adding new physics and phases requires much less modification of the code compared with mesh based methods. Last but not least, the dramatic development of computational power makes it possible to establish a comprehensive model. While current computational capacity may not allow us to have a fully comprehensive model, the easy-extension feature of SPH makes it convenient to keep adding new physics into the model when necessary and computationally feasible.

We have presented in this paper an initial effort and results towards developing a first principle based plume model with comprehensive physics, adopting proper numerical tools and high performance computing. More advanced numerical techniques, such as adaptive particle size, Godunov-SPH, semi-explicit time advancing scheme and better data management strategies and algorithms are on our list to exploit in the future. In the near future, effect of wind field will be take into account. Our code will
5   also be made available in the open source form for the community to enhance.

5.1 Code availability

The Plume-SPH code, together with a user manual providing instructions for installation, running and visualization are archived at https://zenodo.org/record/572819#.WRCy7xiZORs (DOI: 10.5281/zenodo.572819). The input data for all simulations presented in this work are archived in the same repository. Output of simulations presented in this paper are archived in Box.
10 Access permission will be given upon request.

Competing interests. Authors have the standard conflict with employers and listed sponsors

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15 data of PDAC (were also provided by Antonio Costa later together with simulation results of other plume models) which helped us in doing early verification and improvement. We appreciate Antonio Costa for providing simulation results of existing 3D models, which are used in verification and validation section of this paper. We thank Matteo Cerminara for his helping on post-processing of plume simulation results. Computational results reported here were performed at the Center for Computational Research at the University at Buffalo. This project is supported by Grants No. NSF 1131074 from the National Science Foundation.

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